

USE OF BRANCHED MALTODEXTRINS AS GRANULATION BINDERS

The present invention relates to the preparation of granules of active substances containing dietary fiber.

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More particularly, the invention relates to a method for preparing granules of active substances containing dietary fiber, which consists in granulating a mixture of said active substances and branched maltodextrins, said branched maltodextrins contents is of between 3 and 13% by weight of the mixture to be granulated. It is also directed toward the use of these branched maltodextrins as active substance granulation binders.

15 In the context of the present invention, the term "branched maltodextrins" refers to the maltodextrins described in patent application EP 1 006 128, of which the applicant is the proprietor.

20 These branched maltodextrins have between 15 and 35% of 1-6 glucoside linkages, a reducing sugar content of less than 20%, a polymolecularity index of less than 5 and a number-average molecular mass M_n at most equal to 4500 g/mol.

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In addition, the term "active substances" when used herein refers to compounds having dietary and/or pharmaceutical advantages, for instance compounds of the starch or starch derivative type (such as compounds that are generated by acid or enzymatic hydrolysis of starch or compounds that result from the hydrogenation of said starch hydrolysates), or sugars, but also compounds of the strong sweetener type, enzymes, vitamins or pharmaceutical active principles, taken alone or in combination, which exhibit little or no particular capacity for granulation.

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Substances such as proteins, in particular soybean

proteins, are not selected here since they naturally exhibit coagulation properties that are conventionally taken advantage of in order to granulate them.

5 In the food industry, these active substances may be more particularly polysaccharides or oligosaccharides of the dextrin, maltodextrin, polydextrose or fructo-oligosaccharide type, but also polyols, for instance sorbitol, xylitol, mannitol, lactitol, maltitol,
10 erythritol and isomalt.

It is known practice to use these active substances as such, and also as fillers for other active substances such as strong sweeteners, prepared by chemical
15 synthesis, of the saccharin, aspartame, acesulfame K, cyclamate, stevioside, sucralose, neotame or alitame type.

In the pharmaceutical industry, it may be desirable to
20 use these fillers in combination with, for example, pharmaceutical active principles such as antipyretic analgesics, in particular aspirin and its derivatives, paraminophenol derivatives (such as paracetamol) or pyrazolone derivatives.

25 Granulation procedures are often used to take full advantage of the powdered form of these active substances or these mixtures of active substances since it is often desirable to increase their particle size
30 for technical and economic purposes.

The two main reasons for this new formulation are :

- 35 - firstly essentially commercial, given that a granule provides a better appearance and is easier for the user to handle,
- secondly strictly technical, because a granule slots more readily into a rational production process, in terms of being more readily conveyed, of better

flow, of lack of formation of dust, of better homogeneity in a mixture with other substances, etc.

5 However, it is extremely rare to be able to risk direct tableting of an active substance or a mixture of active substances, especially if they are effective at very low doses.

10 It is therefore necessary to formulate these compounds with excipients such as adjuvants (also called granulation binders) in order to confer on the final tablet both mechanical and functional qualities.

15 Two techniques are normally used to obtain a granule: the wet granulation technique and the dry granulation technique.

20 In the case of the wet granulation technique, the product to be granulated, that is either naturally wet because of its upstream production procedure, or artificially wetted with a solvent (water or organic solvent), is in a pasty form at the time of granulation.

25 Two methods are conventionally used for wet granulation: mechanical methods and physical methods.

30 The mechanical methods consist of grinding, rotor granulation or extrusion methods, well known to those skilled in the art.

35 Physical granulation methods that use more natural (and thus less aggressive) product granulation technology, by granulating the product either on itself or on an initiator, are however preferred.

The granulation generators per se are centrifugal force, centripetal force or universal gravity, combined with a granulation binder, conventionally consisting of

water, of a solution of the product to be granulated, of alcohols or of a glaze, etc.

5 The product to be granulated is therefore moved around in a tank, for example by means of a pulsed airflow, or on a spherical disk or with a blade rotor (depending on the product and the effect to be obtained).

10 It continually receives a spray of granulation binders in liquid form to ensure agglomeration.

15 Thus this method makes it possible to prepare a homogeneous mixture by direct contact between the product to be granulated and the granulation binder. Intimate mixing of the two components is then facilitated.

A horizontal rotary knife can subsequently break up the clods of large agglomerates.

20 In this method, which is by far the one most preferred by those skilled in the art, it is however necessary for the granulation binder, once dissolved, to have a suitable viscosity, i.e.:

25 - a sufficiently low viscosity to allow the solution containing the granulation binder to be readily pumped, in order to prevent clogging problems at the outlet of the injection nozzles, so as to promote the formation of fine droplets and to provide an even distribution thereof in the granulation tank,

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- a sufficiently high viscosity to allow the compound to play its role of granulation binder.

35 The dry granulation technique consists of an operation referred to as "compacting" of the powder to be granulated, thus allowing such procedure to be carried out in simple turbines, or compacters, or in reactors under vacuum.

Use is made of methods of the "sintering" type, which bring about superficial fusion of the particles in contact, thus resulting in granulation by
5 agglomeration.

Use is also made of techniques referred to as "agglomeration by hybridization", which consist in combining only mechanically two distinct particles of
10 different size, in general in a ratio of 1 to 10, in such a way that the small particles either become embedded discontinuously at the surface of the large particle or constitute a continuous film encompassing the entire sphere.

15 This technology is preferred when granules of thermo-sensitive active principles must be prepared, since it is known that this method generates only minimal heating, while at the same time promoting mechano-chemical reactions that make it possible to provide
20 good cohesion of the granules.

The granulation binders, depending on their initial particle size, can play this role of large particles
25 that make it possible to attach active substances conventionally having a finer particle size.

Direct association between particles of substances to be granulated and of granulation binders is then
30 promoted.

The drawback of the dry granulation technique is that the subsequent sizing step generates a considerable production of fines.
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The wet granulation technique has the advantage of producing no fines or, if it does produce them, doing so in smaller proportions.

However, the choice of using one or the other approach

depends especially on the nature of the active substance to be granulated and, most particularly, on its behavior during the granulation operations.

5 Subsequently, the definitions of the granulation approach and of the granulation binder for granulating said active substance make it possible to adapt the physical and mechanical qualities of the granule obtained, i.e. its mean diameter, its density, its flow
10 capacity, its residual water content and its friability.

Initial studies were interested in the granulation binder qualities that some active substances might
15 themselves have, and thus do not require the addition of exogenous granulation binders that might alter the quality of said active substance to be granulated (such as the glazes or alcohols mentioned above).

20 Granulation of the active substance is carried out using a diluted solution of this same active substance as a granulation binder.

For example, Velasco et al., in Drug Development and
25 Industrial Pharmacy, 21 (10), 1235-1243, 1995, described the flow properties of maltodextrin powders that could be used as a direct tableting vector.

According to them, the flow parameter of the starting
30 powder is in fact of critical importance for its formulation.

Some maltodextrins, as long as they have satisfactory flow properties, can thus be advantageously used for
35 granulating other compounds, such as active principles of pharmaceutical interest.

Velasco et al. have measured the bulk density, compressibility, dynamic angle of repose and especially

flow capacity parameters of four maltodextrin powders available from the company Grain Processing Corp.

5 Velasco et al. have especially shown that these maltodextrins have completely different flow capacities, depending on the "friction index" parameter of the powder of the maltodextrins under consideration.

10 Some maltodextrins are entirely satisfactory, whereas others, such as Maltrin[®] M 150, do not even pass through the orifice of the device for measuring the flow capacity.

15 This great behavioral heterogeneity of said maltodextrins does not therefore promote their unconditional use in granulation, and therefore only partially facilitates their selection as granulation binders.

20 The other active substances, such as sugars, polyols, strong sweeteners or enzymes, do not have any particular capacities for granulation.

25 Xylitol or mannitol crystals for example show no capacity for direct tableting, neither do strong sweeteners such as aspartame.

For these particular active substances, an exogenous granulation binder is therefore essential for their formulation as granules.

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US patent 5 583 351 describes a method for preparing a dense product based on aspartame in powdered form, which does not have the drawbacks of the starting sweetener, i.e. its poor solubility in water, its
35 tendency to form dust or its strong hygroscopicity.

It does not involve granulating the aspartame as it is, but granulating the aspartame, by centrifugation, extrusion, spheronization or atomization techniques,

with a binder consisting of maltodextrins, of dextrins, of gum arabic, of polyol, of polydextrose or of soluble starch.

- 5 However, it is necessary to introduce up to 40% of this granulation binder. Where maltodextrins are chosen as granulation binders, mixtures must contain from 15 to 25% by weight thereof.
- 10 Another drawback of these granulation binders is that they do not provide the active substance to be granulated with any nutritional plus-value.

It has therefore been recommended to produce granules
15 of these active substances by incorporating dietary fiber into them.

The dietary fiber effects of several soluble starch derivatives have therefore been developed. These fiber
20 effects are the result of both the combination of hydrolysis reactions and transglucosylation reactions which confer on said starch derivatives properties identical to those of dietary fiber (in Englyst and Cummings, American Journal of Clinical Nutrition, 1997,
25 45, pp. 423-431).

Thus, patent application JP No. 2000-37 169, discloses strong sweetener preparations (aspartame, saccharin, sucralose, neotame and derivatives thereof) that have a
30 low energy value, that are not very viscous and that have physiological functions.

These novel low-calorie aspartame preparations are aspartame containing-granules with at least 30% by
35 weight, or even at least 50% by weight, of dietary fiber, which are provided by indigestible dextrins.

The granulation procedure described in patent JP No. 2000-37 169 consist either in atomizing a mixed

aqueous solution of an indigestible dextrin and of a strong sweetener or in creating a core of indigestible dextrins onto which said strong sweetener is sprayed.

5 However, in these two procedures, the indigestible dextrins must be introduced at high concentration. It is even recommended to introduce said indigestible dextrins in proportions reaching virtually the entire mixture.

10

It is in fact acknowledged that these strong sweeteners are active substances that are effective at low dose, given their sweetening power being up to 130 to 8000 times greater than that of sucrose.

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These indigestible dextrins are therefore used as a carrier for active substances, and not as granulation binders. Consequently, they are only intended for granulation of active substances that are effective in very small amounts.

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Patent application US 2002/0146.487 describes the coating of soybean proteins with a thin layer of indigestible carbohydrates, followed by a granulation step with lecithin.

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However, the aim of this method is the production of readily dispersible soybean protein granules.

30 As a matter of fact, Soybean proteins already have excellent granulation capacities (cf. tofu, which is an agglomerated soybean protein).

The coating method is carried out in such a way as to prevent penetration of the carbohydrates into the protein agglomerate. The lecithin is chosen for its surfactant properties used conventionally for promoting protein dispersibility.

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None of these two components is used in the patent

application as a granulation binder, quite the contrary.

5 In view of the foregoing, it appears that there is no simple granulation method using a granulation binder that to provide a solution to the technological constraints of preparing granules of active substances in terms of mechanical stability (flow capacity, friability, rapid dissolution in water, compressibility) and to confer, on the resulting granules, additional nutritional properties (for example dietary fiber effects), without necessarily using large amounts of said granulation binder.

15 To the applicant company's credit, it has succeeded in reconciling these objectives, that are difficult to reconcile, by imaging and developing, at the expense of considerable research, a simple method for preparing granules of active substances containing dietary fiber.

20 The method for preparing granules of active substances containing dietary fiber in accordance with the invention consists in granulating a mixture of said active substances and branched maltodextrins having between 15 and 35% of 1-6 glucoside linkages, a reducing sugar content of less than 20%, a polymolecularity index of less than 5 and a number-average molecular mass M_n at most equal to 4500 g/mol, said branched maltodextrins content being of between 3 and 13% by weight of the mixture to be granulated.

30 These branched maltodextrins are naturally indigestible, which results in the reduction of their calorific value by preventing their assimilation in the small intestine. They are a source of indigestible dietary fiber.

By way of indication, their insoluble fiber content is generally more than 50% on a solids basis, which value

is determined according to the AOAC method No. 985-29 (1986).

Moreover, the low content of molecules with a low
5 degree of polymerization, of said branched malto-
dextrins, also contributes to the reduced caloricity
thereof.

Their high content of 1-6 glucoside linkages results in
10 a decrease in their cariogenic capacity thanks to their
reduced assimilation by the microorganisms leaving in
the oral cavity.

This high level of 1-6 linkages also confers on them
15 entirely specific prebiotic properties: it has in fact
become apparent that the bacteria of the cecum and of
the colon in humans and animals, such as the
butyrogenic, lactic acid or propionic acid bacteria,
metabolize highly branched compounds.

20 Furthermore, these branched maltodextrins promote the
development of beneficial bifidogenic bacteria to the
detriment of undesirable bacteria. This results in
properties that are entirely beneficial to human
25 health.

The applicant company has found that the incorporation
of said branched maltodextrins into a mixture with
active substances makes it possible to prepare granules
30 of said active substances that have both excellent
mechanical properties and physical properties, and also
are a supply of indigestible fiber in applications to
which conventional granulation binders could not
aspire.

35 All the branched maltodextrins described in patent
application EP 1 006 128 are suitable for preparing the
granules of active substances according to the
invention.

According to a preferred variant, said branched maltodextrins have a reducing sugar content of between 2 and 5% and a number-average molecular mass of between 2000 and 3000 g/mol.

According to another advantageous variant, all or some of these branched maltodextrins are hydrogenated.

10 For implementing the method for preparing the granules of active substances containing dietary fiber in accordance with the invention, it is chosen to incorporate from 3 to 13% of branched maltodextrins into the mixture to be granulated.

15 The applicant company has thus overcome a first technical prejudice, by choosing to use these branched maltodextrins in proportions that are conventional for a granulation binder, since it is established in the state of the art that granules containing dietary fiber means granules containing a large proportion of said fiber, to the detriment of the active substance to be granulated.

25 The applicant company has therefore established that the granulation binding capacity of its branched maltodextrins is observed for contents of between 3 and 13% by weight of the final mixture, preferably at a content of 5% by weight.

30 Moreover, as is known by specialists in the technical field of powder granulation, it is essential for the granulation binder to have an excellent capacity for dispersion in solution and a viscosity suited to the technical constraints of the materials used.

The applicant company has therefore overcome another technical prejudice relating to the use of branched maltodextrins as granulation binders, since, as will be

exemplified hereinafter, a relative classification of the viscosities of soluble fibers available on the market indicates that the branched maltodextrins used are among the most viscous solutions of their category.

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Surprisingly and unexpectedly, it has been noted that this viscosity does not in any way impair the formulation of the active substances, whatever the granulation method chosen.

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In a first preferential embodiment of the method in accordance with the invention, the active substances to be granulated are chosen from the group consisting of starches and starch derivatives.

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In a first variant, the starch derivatives are chosen from the group consisting of dextrans, indigestible dextrans, maltodextrins and branched maltodextrins.

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The applicant company has in fact noted that, surprisingly and unexpectedly, the branched maltodextrins used as granulation binders advantageously strengthen the cohesion of the granules consisting of fillers that are themselves conventionally chosen as granulation

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binders. As an illustration of this excellent ability to act as granulation binders of these particular fillers, the applicant company has succeeded in stabilizing the rheological behavior of powders of branched maltodextrins themselves, as will be exemplified hereinafter.

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In a second variant, the starch derivatives are hydrogenated starch hydrolysates or conversion products of the hydrogenated starch hydrolysates, more particularly polyols, even more particularly polyols chosen from the group consisting of sorbitol, mannitol, xylitol and maltitol.

As an illustration of the ability of the branched maltodextrins to act as granulation binders for polyols, trials were undertaken by choosing two polyols
5 that are particularly difficult to granulate, i.e. xylitol and mannitol, as will be exemplified hereinafter.

10 In a second preferential embodiment of the method in accordance with the invention, the active substances to be granulated are chosen from the group consisting of sugars, strong sweeteners, enzymes, vitamins and pharmaceutical active principles.

15 The applicant company chose to granulate the active substances using preferentially wet granulation techniques.

20 A first preferential method of granulation in accordance with the invention therefore consists in:

- 25 - preparing a mixture of powdered active substances with branched maltodextrins that are also powdered, such that said branched maltodextrins content is of between 3 and 13%, preferably approximately 5%, by dry weight relative to the total solids content of the mixture,
- 30 - introducing water in a proportion of 5 to 20%, preferably in a proportion of 10%, by weight of the mixture thus prepared, so as to obtain a homogeneous mixture of wet powders,
- 35 - mechanically agitating the homogeneous mixture of wet powders thus obtained, in a mixer-granulator equipped with a sizing screen,
- recovering and drying the granules as they exit said screen.

The first step of this first method of granulation therefore consists in mixing the active substance to be granulated with from 3 to 13%, preferably of the order of 5%, by dry weight, of branched maltodextrins.

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This operation is carried out by any means known to those skilled in the art. It may be chosen to mix the two components of the mixture in a planetary mixer of the Kenwood type.

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The second step consists in preparing a homogeneous mixture of wet powders. This operation is carried out by introducing water, in a proportion of 5 to 20%, preferably in a proportion of 10%, by weight of the mixture.

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The third step consists in granulating this homogeneous mixture of wet powders in a mixer-granulator equipped with a sizing screen. It may be chosen to carry this step out in a wet granulator of the Erweka FGS type.

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In the final step of this method, the granules obtained are then dried and then sized on said sizing screen.

25 A second preferential method of granulation in accordance with the invention consists in:

- preparing a solution of the branched maltodextrins at a solids content of between 10 and 50%, preferably at a solids content of approximately 25%,

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- spraying the solution of branched maltodextrins thus obtained onto the powder of active substances, in a dryer-granulator, the branched maltodextrins content is of between 3 and 13%, preferably approximately 5%, by dry weight, of the total solids content of the mixture,

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- recovering and drying the granules thus obtained.

The first step of this second method of granulation therefore consists in first of all preparing a solution of branched maltodextrins at a solids content of between 10 and 50%, preferably at a solids content of 25%.

The natural properties of rapid dissolution of the branched maltodextrins, greater than those of the standard equivalent maltodextrins, promote their solubilization at such a solids content.

The second step consists in spraying the resulting solution of branched maltodextrins onto the powder of active substances, the branched maltodextrins content is of between 3 and 13%, preferably 5%, by dry weight of the total solids content of the mixture. This procedure can advantageously be carried out in a dryer-granulator with a fluidized airbed of the Strea-1 type from Aeromatic, equipped with an injecting nozzle.

Despite the relative dynamic viscosity of the resulting maltodextrin solution, the applicant company did not notice any unfortunate problems :

- of pumping of the solution of this granulation binder,
- of spraying at the outlet of the nozzles for injecting the liquid into the mass of particles of active substances moving in the granulator-mixer,
- of heterogeneity of the produced mixture,
- of disparity in the distribution of the droplets of the projected granulation binder.

The third step of this method consists, finally, in recovering and drying the resulting granules, by any means known to those skilled in the art.

This ability of the branched maltodextrins having between 15 and 35% of 1-6 glucoside linkages, a reducing sugar content of less than 20%, a polymolecularity index of less than 5 and a number-average molecular mass M_n at most equal to 4500 g/mol to readily granulate various active substances leads quite naturally to their use as granulation binders for preparing granules of active substances.

Other characteristics and advantages of the present invention will emerge clearly on reading the examples given hereinafter, which illustrate the invention without however limiting it.

Example 1

The relative viscosity of solutions of soluble fibers available on the market, that are capable of providing, as granulation binder, the granules of active substances with a nutritional component was determined in the following way.

The viscosity of these various products was measured by means of an Ares strain-controlled rotary rheometer (Rheometric Scientific) equipped with geometry of the cone-plate type. A shear gradient is applied to the product and the constraint (rotation couple) necessary for the shear is measured. The viscosity measurements (η) are expressed, in Pa.s, by the ratio between the constraint and the shear gradient. The measuring system is thermostatted and the temperature is maintained at $\pm 0.1^\circ\text{C}$.

Solutions containing a solids content of 25% of each of the commercial fibers are prepared, and the viscosity of said solutions is measured at a temperature of 20°C .

Table I below gives the relative viscosity of the branched maltodextrins chosen as granulation binders

according to the invention, with regard to polydextrose, indigestible dextrans, fructo-oligosaccharides and galacto-oligosaccharides that are commercially available.

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The viscosity index was set at 1 for the branched maltodextrins having a reducing sugar content of between 2 and 5% and a number-average molecular mass of between 2000 and 3000 g/mol used in the invention.

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Table I. Relative classification of the viscosities of the soluble fibers of the market

Name of the soluble fiber	Producer	Molecule type	Viscosity index
Litesse II	Cultor	Polydextrose	0.6
Pine fiber	Matsutani	Indigestible dextrin	0.4
Litesse I	Cultor	Polydextrose	0.3
Litesse III	Cultor	Polydextrose	0.2
Actilight 950 P	Beghin Meiji	Fructo-oligosaccharide	0.2
Cup Oligo P	Nisshin Seito	Galacto-oligosaccharide	0.2
Raftilose P95	Orafti	Fructo-oligosaccharide	0.2

15 It clearly appears that the branched maltodextrins used here have the highest viscosity index of their category, which means that they would not naturally be intended for use as granulation binders.

Example 2

In order to illustrate the ability of the branched maltodextrins to be able to act as granulation binders, said branched maltodextrins described in example 1 are granulated on themselves.

This ability of the branched maltodextrins to act as a granulation binder should improve their physical and mechanical properties, or even erase the deficiencies of the initial branched maltodextrin powder, in particular in terms of dust production.

A solution of branched maltodextrins with a 25% solids content (25 g of branched maltodextrins with 75 g of water) is prepared.

475 g of a branched maltodextrin powder having a mean particle size of 77 μm are placed in the bowl of the Aeromatic Strea-1 fluidized airbed dryer-granulator equipped with an injecting nozzle.

By means of air pulsed at the base of the bowl, the powder is suspended at a temperature of 60°C. The solution of branched maltodextrins is then sprayed at a flow rate of 4 ml/min and a pressure of 1 bar.

The granules recovered after 25 to 30 min of elapsed time are recovered and dried in the granulator for 30 minutes at 60°C. The granules are then sized on a sieve having a 1250 μm mesh size.

The particle size, the flow capacity, the aerated density and the compressibility of the resulting granules are then measured. A dust test is also carried out in order to determine the cohesion of the granules.

The size of the granules is measured on a Coulter[®] LS laser particle sizer, and is expressed by the arith-

metic mean of the sizes of the particles (μm) obtained.

The flow of the granules is determined by means of a "funnel" test according to the pharmaceutical technical method 2.9.16 of the European Pharmacopeia, 3rd edition, and which consists in measuring the flow rate, expressed in seconds, of 100 g of granules deposited into a funnel whose dimensions are precisely given in this method.

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The aerated density is, for its part, measured by means of a graduated cylinder test, which consists in using a 250 ml cylinder graduated every 2 ml. 100 g of granules weighed out with a precision of 0.5% are introduced without tapping into the dry cylinder. The apparent untapped volume V_0 , estimated to within 1 ml, is then read.

The aerated density measured here corresponds to the ratio of the weight of granules (here 100 g) to the volume measured with the cylinder (V_0).

The compressibility measurement consists in determining the strength, expressed in Newtons, which corresponds to the resistance to the crushing of tablets, measured on a Schleuniger 2E durometer.

These tablets, produced on a Frogerais/Sviac alternating press equipped with concave punches 13 mm in diameter, from a mixture of 99.5% of granules in accordance with the invention and of 0.5% of magnesium stearate, are cylindrical in shape with convex faces (radius of curvature 13 mm), having a diameter of 13 mm, a thickness of 6 mm and a weight equal to 0.771 g, i.e. having a volume of 0.571 cm^3 and an apparent density of 1.35 g/cm^3 .

Finally, the dust test consists in measuring the ability of a granule to release fine particles into a

calibrated stream of air. For this measurement, a Heubach-Dustmeter device assembled in its type II configuration is used. 100 g of granules are introduced into the device, and subjected to a stream of air at a flow rate of 8 l/min for 5 min, at a temperature of 20°C.

The fine particles drifted by this stream of air are collected on a filter paper which is then weighed. The dust test consists in determining the weight of fine particles accumulated on the surface of the filter.

Table II below gives the results obtained on the granules of branched maltodextrins in accordance with the invention (granules A), in comparison with the initial powder of branched maltodextrins. Given as a control, are the results of the analyses carried out on the granules (granules B) obtained by taking, as granulation binder, a particular maltodextrin, sold by the applicant company under the brand name Lycatab[®] DSH as wet granulation excipient, instead of the branched maltodextrins, and carrying out the process in exactly the same way as for obtaining the granules A.

Table II. Results of analyses of the granules obtained

	Starting branched maltodextrins	Granules A	Granules B
Particle size (µm)	77	160	136.5
Flow of powder (s)	8	9	10
Apparent density (g/ml)	0.375	0.393	0.387
Compressibility (N)	250	190	195
Dust test (g)	0.0925	0.0221	0.0325

Granulation of the branched maltodextrins on themselves makes it possible to notably reduce the dust generated by the handling of the initial branched maltodextrin powders, while at the same time making it possible to

obtain granules for which the flow capacity, the density and the compressibility are in accordance with what can be expected of an effective granulation binder, since the values are equivalent to those
5 obtained with Lycatab[®] DSH.

Example 3

Crystalline xylitol sold by the applicant company under
10 the brand name Xylisorb[®] 300 (mean particle size of 175.8 μ m) is granulated with the branched maltodextrins of example 1, under the same conditions as those described in example 2.

15 Table III below gives the results of the analyses carried out on the xylitol granules prepared with the branched maltodextrins as granulation binders (granules C), in comparison with the starting xylitol powder.

20 Given as a control, are the results of the analyses carried out on granules obtained by also taking Lycatab[®] DSH as wet granulation binder, instead of the branched maltodextrins (granules D).

25 Table III. Results of analyses of the granules obtained

	Starting Xylisorb [®] 300	Granules C	Granules D
Particle size (μ m)	175.8	229	256
Flow of powder(s)	infinite	11	13
Apparent density (g/ml)	0.583	0.578	0.521
Compressibility (N)	ND [*]	130	120
Dust test (g)	0	0.0014	0.0024

ND^{*}: not detectable

30 The granulation of the xylitol using the branched maltodextrins as granulation binders, just like the granulation carried out with Lycatab[®] DSH, make it

possible to confer on the xylitol flow properties that it absolutely does not possess. This granulation is, moreover, the only way to confer on xylitol a satisfactory compressibility.

5

It should, however, be noted that, in addition to their additional supply of dietary fiber, the branched maltodextrins used as granulation binders improve the flow of the xylitol granules and limit slightly more the formation of dust, compared with Lycatab[®] DSH taken as conventional granulation binder.

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Example 4

15 Crystalline mannitol is granulated with the branched maltodextrins of example 1.

950 g of crystalline mannitol sold by the applicant company under the name Mannitol P60 (mean particle size of 60 μ m) are mixed with 50 g of a branched maltodextrin powder in a planetary mixer of the Kenwood type at minimum speed for 5 minutes.

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Water is added in a proportion of 10 parts of water per 100 parts of the mixture thus obtained, and mixing is continued for 10 minutes.

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The granulation is then carried out on an Erweka FGS wet granulator equipped with a 1000 μ m screen, according to the constructor's specifications.

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The granules obtained are then dried in an Aeromatic Strea-1 laboratory fluidized airbed dryer at a temperature of 60°C for 30 min. The granules are then sized on said 1000 μ m sizing screen (granules E).

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As a control, Mannitol P60 is granulated with 5% of Lycatab[®] DSH, as wet granulation excipient (granules F), under the same operating conditions.

The results of the comparative measurements of the granules obtained with these two granulation binders, in terms of powder density, of flow time and of compressibility, carried out under conditions identical to examples 2 and 3, are given in table IV below.

The particle size measurements are here carried out on a Fritsch Analysette 3 laboratory electromagnetic sieving device, and are expressed as mean particle diameter (size of 50% of total particles).

Table IV. Results of analyses of the granules obtained

	Starting Mannitol P60	Granules E	Granules F
Particle size (μm)	60	860	860
Flow of powder(s)	infinite	13	13
Apparent density (g/ml)	0.588	0.540	0.550
Compressibility (N)	ND [*]	80	80

The granulation of the crystalline mannitol with the branched maltodextrins as granulation binders makes it possible to obtain granules for which the flow capacity, the density and the compressibility are in accordance with what can be expected from an effective granulation binder, since the values are equivalent to those obtained with Lycatab[®] DSH. The intrinsic nature of the branched maltodextrins as dietary fiber can thus be fully taken advantage of, in addition to their properties as granulation binders.